## Thermodynamics Ph.D. Qualifying Exam

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Directions: Closed book. One sheet of notes allowed. Formula sheet/tables provided. All problems carry equal weight. In order to receive full credit for a solution, you must show all work clearly.

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1. Air is in a piston-cylinder assembly, initially at $\mathrm{p}=6.75 \mathrm{bar}, \mathrm{T}=600 \mathrm{~K}, \mathrm{~V}=0.5 \mathrm{~m}^{3}$. The air is expanded to 1.32 bar in an adiabatic process. The process occurs internally reversibly. You can assume that the air is an ideal gas and that changes in KE and PE for the system are negligible. (10 points)
a) What is the final temperature of the air, in K ?

b) What is the work done during the process, in kJ ?
2. Air enters the diffuser of a turbojet engine with a mass flow rate of $25 \mathrm{~kg} / \mathrm{s}$ at $30 \mathrm{kPa}, 250 \mathrm{~K}$, and a velocity of $142 \mathrm{~m} / \mathrm{s}$. Then property data of the air at various states within the engine is listed below. The diffuser, compressor, and nozzle operate internally reversibly, but the turbine has irreversibilities. For the problem, assume ideal gas behavior and air-standard analysis. (10 points)

| STATE | $\underset{(k P a)}{\mathbf{p}}$ | T | $\begin{gathered} \mathrm{h} \\ (\mathrm{~kJ} / \mathrm{kg}) \end{gathered}$ | $\begin{gathered} \mathbf{v} \\ (\mathrm{m} / \mathrm{s}) \end{gathered}$ | $\begin{gathered} \mathbf{s}^{\circ} \\ \left(\mathrm{kJ} / \mathrm{kg}^{\star} \mathrm{K}\right) \end{gathered}$ | $\begin{gathered} \text { If } \boldsymbol{\Delta} \mathbf{s}=\mathbf{0} \\ \hline \mathrm{p}_{\mathrm{r}} \text { (relative } \\ \text { pressure) } \end{gathered}$ |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: |
|  |  |  |  |  |  |  |
| a | 30 | $\begin{gathered} 250 \\ \mathrm{~K} \end{gathered}$ | 250.05 | 142 | 1.51917 | . 7329 |
| 1 | 38.4 | $\begin{gathered} 260 \\ K \end{gathered}$ | 260.09 | 0 | 1.55848 | . 8405 |
| 2 | 480 | $\begin{gathered} 532 \\ K \end{gathered}$ | 536.01 | 0 | 2.28355 | 10.5 |
| 3 | 480 | $\begin{gathered} 1120 \\ \mathrm{~K} \end{gathered}$ | 1184.28 | 0 | 3.09825 | 179.7 |
| 4 | 38.4 | $\begin{gathered} 600 \\ K \end{gathered}$ | 607.02 | 0 | 2.40902 | 16.28 |
| 5 | 30 | $\begin{gathered} 560 \\ K \end{gathered}$ | 568.17 |  | 2.33685 | 12.7 |


a) The data in the table are for real operation of the turbojet. What is the isentropic efficiency of the turbine, $\eta_{T}$ ?
b) What is the velocity at the nozzle exit for real (irreversible) operation, in $\mathrm{m} / \mathrm{s}$ ?
3. A solar-powered heat pump receives energy as heat from a solar collector at $T_{H}$, rejects heat to the surroundings at $T_{A}$, and pumps heat from a cold space at $T_{C}$, with no other external energy transfers.
A) If the three heat transfer rates are $Q_{H}, Q_{A}$, and $Q_{C}$, find an expression for the minimum ratio $Q_{H} / Q_{C}$, in terms of the three temperatures.
B) If $\mathrm{T}_{\mathrm{H}}=350 \mathrm{~K}, \mathrm{~T}_{\mathrm{A}}=290 \mathrm{~K}, \mathrm{~T}_{\mathrm{C}}=200 \mathrm{~K}$, and $\mathrm{Q}_{\mathrm{C}}=10 \mathrm{~kW}$, and each $\mathrm{m}^{2}$ of the solar collector captures 0.2 kW , what is the minimum solar collector area required?
4. A well-insulated tank whose volume is $0.35 \mathrm{~m}^{3}$ is initially evacuated. A valve connects the tank to a supply line of $\mathrm{H}_{2} \mathrm{O}$, which is a saturated vapor at 10 bar. The valve is opened and the vapor flows into the tank until the pressure inside is 1.5 bar. There is no work during this process. (10 points)
a) Determine the temperature of the $\mathrm{H}_{2} \mathrm{O}$ in the tank when the process is complete ( $\mathrm{p}=1.5 \mathrm{bar}$ ).

b) Determine the mass of $\mathrm{H}_{2} \mathrm{O}$ contained in the tank when the process is complete.
c) Determine the amount of entropy generated in the process $\left(\sigma_{g e n}\right)$, in $\mathrm{kJ} / \mathrm{K}$.

## TABLE A-4

## TABLE A-22

$T(\mathrm{~K}), h$ and $u(\mathrm{~kJ} / \mathrm{kg}), s^{\circ}(\mathrm{kJ} / \mathrm{kg} \cdot \mathrm{K})$

## Ideal Gas Properties of Air

| $T$ | $h$ | $u$ | $s^{0}$ | when $\Delta s=0$ $p_{r} \quad v_{r}$ |  |
| :---: | :---: | :---: | :---: | :---: | :---: |
| 350 | 350.49 | 250.02 | 1.85708 | 2.379 | 422.2 |
| 360 | 360.58 | 257.24 | 1.88543 | 2.626 | 393.4 |
| 370 | 370.67 | 264.46 | 1.91313 | 2.892 | 367.2 |
| 380 | 380.77 | 271.69 | 1.94001 | 3.176 | 343.4 |
| 390 | 390.88 | 278.93 | 1.96633 | 3.481 | 321.5 |
| 400 | 400.98 | 286.16 | 1.99194 | 3.806 | 301.6 |
| 410 | 411.12 | 293.43 | 2.01699 | 4.153 | 283.3 |
| 420 | 421.26 | 300.69 | 2.04142 | 4.522 | 266.6 |
| 430 | 431.43 | 307.99 | 2.06533 | 4.915 | 251.1 |
| 440 | 441.61 | 315.30 | 2.08870 | 5.332 | 236.8 |
| 580 | 586.04 | 419.55 | 2.37348 | 14.38 | 115.7 |
| 590 | 596.52 | 427.15 | 2.39140 | 15.31 | 110.6 |
| 600 | 607.02 | 434.78 | 2.40902 | 16.28 | 105.8 |
| 610 | 617.53 | 442.42 | 2.42644 | 17.30 | 101.2 |

Properties of Superheated Water Vapor

| T | $v$ | $u$ | $h$ | $s$ |
| :---: | :---: | :---: | :---: | :---: |
| ${ }^{\circ} \mathrm{C}$ | $\mathrm{m}^{3} / \mathrm{kg}$ | kJ/kg | kJ/kg | kJ/kg $\cdot \mathrm{K}$ |


| $p=1.5 \mathrm{bar}=0.15 \mathrm{MPa}$ |  |  |  |  |  |
| :--- | :---: | :---: | :---: | :---: | :---: |
|  | $\left(T_{\text {sat }}=111.37^{\circ} \mathrm{C}\right)$ |  |  |  |  |,


| TABLE A-3 |  |  |  |  |  |  |  |  |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
|  |  | Properties of Saturated Water (Liquid-Vapor): Pressure Table |  |  |  |  |  |  |  |  |  |
| Pressure Conversions:$\begin{aligned} 1 \mathrm{bar} & =0.1 \mathrm{MPa} \\ & =10^{2} \mathrm{kPa} \end{aligned}$ |  | Specific Volume $\mathrm{m}^{3} / \mathrm{kg}$ |  | Internal Energy kJ/kg |  | Enthalpy kJ/kg |  |  | Entropy <br> kJ/kg K |  |  |
| Press. bar | Temp. ${ }^{\circ} \mathrm{C}$ | Sat. <br> Liquid $v_{\mathrm{f}} \times 10^{3}$ | Sat. <br> Vapor <br> $v_{g}$ $\qquad$ | Sat. Liquid $u_{\mathrm{f}}$ | Sat. <br> Vapor <br> $u_{\mathrm{g}}$. | Sat. Liquid $h_{f}$ | Evap. $\boldsymbol{h}_{\mathrm{fg}} .$ | Sat. <br> Vapor $h_{\mathrm{g}}$ | Sat. Liquid $S_{f}$ | Sat. <br> Vapor <br> $S_{g}$ | Press. bar |
| 1.50 | 111.4 | 1.0528 | 1.159 | 466.94 | 2519.7 | 467.11 | 2226.5 | 2693.6 | 1.4336 | 7.2233 | 1.50 |
| 2.00 | 120.2 | 1.0605 | 0.8857 | 504.49 | 2529.5 | 504.70 | 2201.9 | 2706.7 | 1.5301 | 7.1271 | 2.00 |
| 10.0 | 179.9 | 1.1273 | 0.1944 | 761.68 | 2583.6 | 762.81 | 2015.3 | 2778.1 | 2.1387 | 6.5863 | 10.0 |
| 15.0 | 198.3 | 1.1539 | 0.1318 | 843.16 | 2594.5 | 844.84 | $1947 \cdot 3$ | 2792.2 | 2.3150 | 6.4448 | 15.0 |

